## **Claims**

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- 1. A process for preparing at least one olefin having from 8 to 12 carbon atoms from at least one olefin having from 4 to 6 carbon atoms by means of a four-stage synthesis, which comprises
- a) hydroformylating at least one starting olefin in the first process step,
  - b) hydrogenating the at least one aldehyde obtained in the first step a) to form the corresponding alcohol,
  - c) preparing at least one 1-olefin by elimination of water from the at least one alcohol obtained in the second process step b) and
- d) obtaining at least one olefin by metathesis with elimination of ethylene from the at least one 1-olefin(s) obtained in the third process step c).
  - 2. The process as claimed in claim 1, wherein a mixture of olefins having from 4 to 6 carbon atoms is used and a mixture of olefins having from 8 to 12 carbon atoms is obtained.
  - 3. The process as claimed in claim 1 or 2, wherein a nickel, copper, copper/nickel, copper/chromium, copper/chromium/nickel, zinc/chromium, nickel/molybdenum catalyst is used as catalyst in the second process step b).
  - 4. The process as claimed in at least one of claims 1 to 3, wherein the elimination of water in the third process step c) is carried out continuously over a solid catalyst which consists formally of aluminum oxide and barium oxide.
  - 5. The process as claimed in at least one of claims 1 to 4, wherein a rhenium catalyst comprising Re<sub>2</sub>O<sub>7</sub> on γ-Al<sub>2</sub>O<sub>3</sub> or on mixed supports selected from among SiO<sub>2</sub>/Al<sub>2</sub>O<sub>3</sub>, B<sub>2</sub>O<sub>3</sub>/SiO<sub>2</sub>/Al<sub>2</sub>O<sub>3</sub> or Fe<sub>2</sub>O<sub>3</sub>/Al<sub>2</sub>O<sub>3</sub> is used in the fourth process step d).
  - 6. The process as claimed in at least one of claims 1 to 5,

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wherein a hydrocarbon stream comprising or consisting of isobutene and linear butenes is used as starting material in process step a).

- 7. The process as claimed in at least one of claims 1 to 6, wherein a C<sub>4</sub> fraction selected from among raffinate I, selectively hydrogenated C<sub>4</sub> fraction from a cracker, C<sub>4</sub> fractions from FCC plants or C<sub>4</sub>-olefins prepared by the Fischer-Tropsch synthesis is used as starting material.
- 8. The process as claimed in at least one of claims 1 to 7,
  wherein industrial C<sub>4</sub> fractions having an isobutene content of greater than 3% by weight are used as starting material.
  - 9. The process as claimed in at least one of claims 6 to 8, wherein 3-methyl-1-butene is separated off from the 1-olefin fraction comprising olefins having 5 carbon atoms which is obtained after the third process step c).
  - 10. A mixture which comprises at least one olefin having from 8 to 12 carbon atoms and has been prepared by a process as claimed in any of claims 1 to 9.
- 20 11. Isooctene prepared by a process as claimed in any of claims 1 to 9 using a C<sub>4</sub> fraction having an isobutene content of greater than 3% by weight as starting material.
  - 12. The use of a mixture as claimed in claim 10 or of isooctene as claimed in claim 11 for preparing alcohols and/or aldehydes.
  - 13. The use as claimed in claim 12 for preparing plasticizer alcohols.
  - 14. The use as claimed in claim 12 for preparing isononanol.